BUILDING AIR INTAKE AND EXHAUST DESIGN

FRESH air enters a building through its air intake. Likewise, building exhausts remove air contaminants from a building so wind can dilute the emissions. If the intake or exhaust system is not well designed, contaminants from nearby outside sources (e.g., vehicle exhaust) or from the building itself (e.g., laboratory fume hood exhaust) can enter the building with insufficient dilution. Poorly diluted contaminants may cause odors, health impacts, and reduced indoor air quality. This chapter discusses proper design of exhaust stacks and placement of air intakes to avoid adverse air quality impacts. Chapter 16 of the 2001 *ASHRAE Handbook—Fundamentals* more fully describes wind and airflow patterns around buildings. Related information can also be found in Chapters 7, 14, 29, 30, and 31 of this volume, Chapters 12 and 13 of the 2001 *ASHRAE Handbook—Fundamentals*, and Chapters 24, 25, and 30 of the 2000 *ASHRAE Handbook—HVAC Systems and Equipment*.

EXHAUST STACK AND AIR INTAKE DESIGN STRATEGIES

Stack Design Strategies

The dilution a stack exhaust can provide is limited by the dispersion capability of the atmosphere. Before discharge, exhaust contamination should be reduced by filters, collectors, and scrubbers.

Central exhausts that combine flows from many collecting stations should always be used where safe and practical. By combining several exhaust streams, central systems dilute intermittent bursts of contamination from a single station. Also, the combined flow forms an exhaust plume that rises a greater distance above the emitting building. Additional air volume can be added to the exhaust near the exit with a makeup air unit to increase initial dilution and exhaust plume rise. This added air volume does not need heating or cooling, saving on energy costs.

In some cases, separate exhaust systems are mandatory. The nature of the contaminants to be combined, recommended industrial hygiene practice, and applicable safety codes need to be considered. Separate exhaust stacks could be grouped in a tight cluster to take advantage of the larger plume rise of the resulting combined jet. Also, a single stack location for a central exhaust system or a tight cluster of stacks allows building air intakes to be positioned as far as possible from the exhaust. For a tight cluster to be considered as a single stack in dilution calculations, the stacks must be uncapped, have approximately the same exhaust velocities, and all lie within a two-stack diameter radius of the middle of the group. Stacks lined up in a row do not act as a single stack (Gregoric et al. 1982).

As shown in Figure 1, the stack height h_s is measured above the roof level on which the air intake is located. Wilson and Winkel (1982) demonstrated that stacks terminating below the level of adjacent walls and architectural enclosures frequently do not effectively reduce roof-level exhaust contamination. To take full advantage of their height, stacks should be located on the highest roof of a building.

Architectural screens used to mask rooftop equipment adversely affect exhaust dilution, depending on porosity, relative height, and
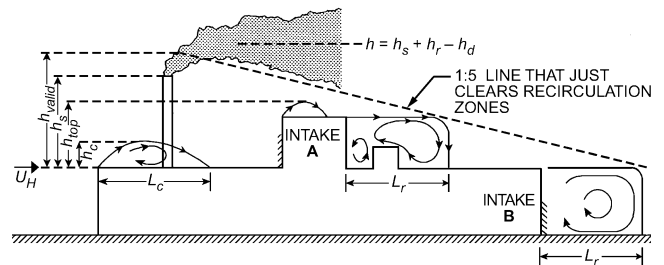
Fig. 1   Flow Recirculation Regions and Exhaust-to-Intake Stretched-String Distances
(Wilson 1982)

distance from the stack. Petersen et al. (1998) found that exhaust dispersion improves with increased screen porosity.

Large buildings, structures, and terrain close to the emitting building can adversely affect stack exhaust dilution, because the emitting building can be within the recirculation flow zones downwind of these nearby flow obstacles (Wilson et al. 1998a). In addition, an air intake located on a nearby taller building can be contaminated by exhausts from the shorter building. Wherever possib.le, facilities emitting toxic or highly odorous contaminants should not be located near taller buildings or at the base of steep terrain.

As shown in Figure 2, stacks should be vertically directed and uncapped. Stack caps that deflect the exhaust jet have a detrimental effect on the exhaust plume rise. Small conical stack caps often do not completely exclude rain, because rain does not usually fall straight down; periods of heavy rainfall are often accompanied by high winds that deflect raindrops under the cap and into the stack (Changnon 1966). A stack exhaust velocity V_e of about 13 m/s prevents condensed moisture from draining down the stack and keeps rain from entering the stack. For intermittently operated systems, protection from rain and snow should be provided by stack drains, as shown in Figure 2F to 2J, rather than stack caps.

Recommended Stack Exhaust Velocity

High stack exhaust velocity and temperatures increase plume rise, which tends to reduce intake contamination. The exhaust velocity V_e should be maintained above 10 m/s (even with drains in the stack) to provide adequate plume rise and jet dilution. Velocities above 10 m/s provide still more plume rise and dilution, but above 15 to 20 m/s, noise and vibration from exhaust fans becomes an important concern. An exit nozzle (Figure 2B) can be used to increase exhaust velocity and plume rise.

An exception to these exhaust velocity recommendations may be when corrosive condensate droplets are discharged. In this case, a velocity of 5 m/s in the stack and a condensate drain are recommended to reduce droplet emission. At this low exhaust velocity, an exit nozzle should be used to avoid plume downwash (Figure 2B).

Stack wake downwash occurs where low-velocity exhausts are pulled downward by negative pressures immediately downwind of the stack, as shown in Figure 3. V_e should be at least 1.5 times the design speed U_H at roof height in the approach wind to avoid stack
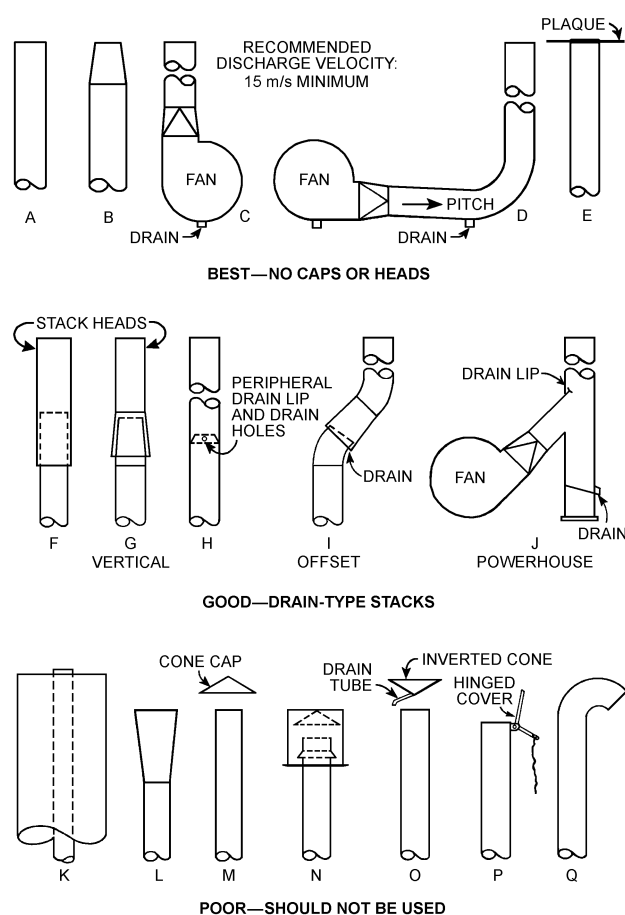
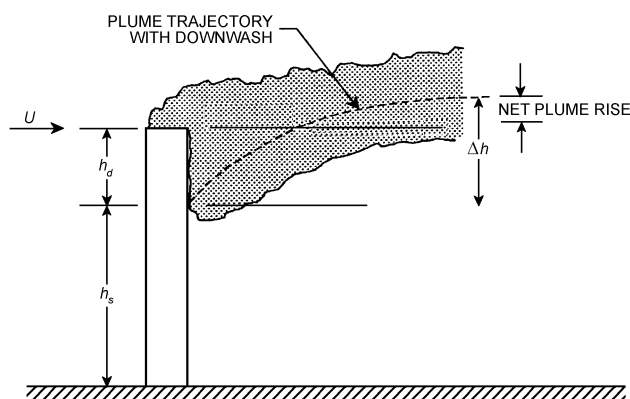**Fig. 2 Stack Designs Providing Vertical Discharge and Rain Protection**

Fig. 3 Reduction of Effective Stack Height by Stack Wake Downwash

wake downwash. A meteorological station design wind speed U_{met} that is exceeded less than 1% of the time can be used. This value can be obtained from Tables 1A, 2A, or 3A in Chapter 27 of the 2001 *ASHRAE Handbook—Fundamentals*, or estimated by applying Table 2 of Chapter 16 of that volume to annual average wind speed. Because wind speed increases with height, a correction for roof height should be applied for buildings significantly higher than 10 m, using Equation (4) and Table 1 of Chapter 16 of the 2001 *ASHRAE Handbook—Fundamentals*.

Other Stack Design Standards

Minimum heights for chimneys and other flues are discussed in the *Uniform Building Code* (ICBO 1994). For laboratory fume hood exhausts, American Industrial Hygiene Association (AIHA) *Standard* Z9.5 recommends a minimum stack height of 3 m above the adjacent roof line, an exhaust velocity V_e of 15 m/s, and a stack height extending one stack diameter above any architectural screen; National Fire Protection Association (NFPA) *Standard* 45 specifies a minimum stack height of 3 m to protect rooftop workers. Toxic chemical emissions may also be regulated by federal, state, and local air quality agencies.

Air Intake Locations to Minimize Contamination

Carefully placed outside air intakes can reduce stack height requirements and help maintain acceptable indoor air quality. Rock and Moylan (1999) review recent literature on air intake locations and design. Petersen and LeCompte (2002) also showed the benefit of placing air intakes on building sidewalls.

ASHRAE *Standard* 62, Ventilation for Acceptable Indoor Air Quality, highlights the need to locate makeup air inlets and exhaust outlets to avoid contamination. The following sections describe various outside contamination sources to consider:

Toxic Stack Exhausts. Boilers, emergency generators, and laboratory fume hoods are some sources that can seriously affect building indoor air quality because of toxic air pollutants. These sources, especially diesel-fueled emergency generators, can also produce strong odors that may require administrative measures, such as generator testing during low building occupancy or temporarily closing the intakes.

Automobile and Truck Traffic. Heavily traveled roads and parking garages emit carbon monoxide, dust, and other pollutants. Diesel trucks and ambulances are common sources of odor complaints (Smeaton et al. 1991). Intakes near vehicle loading zones should be avoided. Overhead canopies on vehicle docks do not prevent hot vehicle exhaust from rising to intakes above the canopy. When the loading zone is in the flow recirculation region downwind from the building, vehicle exhaust may spread upwind over large sections of the building surface (Ratcliff et al. 1994). Garbage containers may also be a source of odors, and garbage trucks may emit diesel exhaust with strong odors.

Kitchen Cooking Hoods. Kitchen exhaust can be a source of odors and cause plugging and corrosion of heat exchangers. Grease hoods have stronger odors than other general kitchen exhausts. Grease and odor removal equipment beyond that for code requirements may be needed if air intakes cannot be placed far away.

Evaporative Cooling Towers. Outbreaks of Legionnaires' disease have been linked to bacteria in cooling tower drift droplets being drawn into the building through air intakes (Puckorius 1999). ASHRAE *Guideline* 12 gives advice on cooling tower maintenance for minimizing the risk of Legionnaires' disease, and suggests keeping cooling towers as far away as possible from intakes, operable windows, and outside public areas. No specific minimum separation distance is provided or available. Prevailing wind directions should also be considered to minimize risk. Evaporative cooling towers can have several other effects: water vapor can increase air-conditioning loads, condensing and freezing water vapor can damage equipment, and ice can block intake grilles and filters. Chemicals added to retard scaling and biological contamination may be emitted from the cooling tower, creating odors or health effects, as discussed by Vanderheyden and Schuyler (1994).

Building General Exhaust Air. General indoor air that is exhausted will normally contain elevated concentrations of carbon dioxide, dust, copier toner, off-gassing from materials, cleaning agents, and body odors. General exhaust air should not be allowed to reenter the building without sufficient dilution.

Stagnant Water Bodies, Snow, and Leaves. Stagnant water bodies can be sources of objectionable odors and potentially harmful organisms. Poor drainage should be avoided on the roof or ground near the intake. Restricted airflow from snow drifts, fallen leaves, and other debris can be avoided in the design stage with elevated louvers above ground or roof level.

Rain and Fog. Direct intake of rain and fog can increase growth of microorganisms in the building. AMCA (1993) recommends selecting louvers and grilles with low rain penetration and installing drains just inside the louvers and grilles. In locations with chronic fog, some outside air treatment is recommended. One approach is to recirculate some part of the indoor air to evaporate entrained water droplets, even during full air-side economizer operation (maximum outside air use).

Environmental Tobacco Smoke. Outside air intakes should not be placed close to outside smoking areas.

Plumbing Vents. Codes frequently require a minimum distance between plumbing vents and intakes to avoid odors.

Smoke from Fires. Smoke from fires is a significant safety hazard because of its direct health effects and from reduced visibility during evacuation. NFPA *Standard* 92A-1996, Recommended Practice for Smoke-Control Systems (Section 2-3.3.1), discusses the need for good air intake placement relative to smoke exhaust points.

Construction. Construction dust and equipment exhaust can be a significant nuisance over a long period. Temporary preconditioning of outside air is necessary in such situations, but is rarely provided. A simple solution is to provide room and access to the outside air duct for adding temporary air treatment filters or other devices, or a sufficient length of duct so that such equipment could be added when needed. Intake louvers and outside air ducts also require more frequent inspections and cleaning when construction occurs nearby.

Vandalism and Terrorism. Acts of vandalism and terrorism are of increasing concern. Louvers and grilles are potential points of illegal access to buildings, so their placement and construction are important. Intentional introduction of offensive or potentially harmful gaseous substances is also of concern. Some prudent initial design considerations might be elevating the grilles and louvers away from easy pedestrian access and specifying security bars and other devices. Also, the unlocked stair tower doors required for roof access during emergency evacuations may limit use of rooftop air intakes in sensitive applications because individuals would have ready access to the louvers. For more information, see ASHRAE (2003), Risk Management Guidance for Health, Safety, and Environmental Security under Extraordinary Incidents.

General Guidance on Intake Placement

Experience provides some general guidelines on air intake placement. As a rule, intakes should never be located in the same architectural screen enclosure as contaminated exhaust outlets, especially low-momentum exhausts (which tend to be trapped in the wind recirculation zone within the screen). For more information see the section on Influence of Architectural Screens on Exhaust Dilution.

If exhaust is discharged from several locations on a roof, intakes should be sited to minimize contamination. Where all exhausts of concern are emitted from a single, relatively tall stack or tight cluster of stacks, a possible intake location might be close to the base of this tall stack, if this location is not adversely affected by other exhaust locations. However, contaminant leakage from the side of the stack has been observed in positively pressurized areas between the exhaust fans and stack exit (Hitchings 1997; Knutson 1997), so air intakes should not be placed very close to highly toxic or odorous exhaust stacks regardless of stack height.

Intakes near vehicle loading zones should be avoided. Overhead canopies on vehicle docks do not effectively protect air intakes, and vehicle exhaust may spread over large sections of the building surface. Loading zones also may have garbage and solid waste receptacles that create odors; trucks that serve the receptacles also
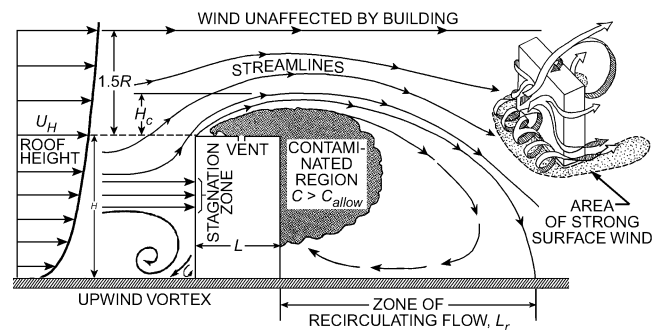

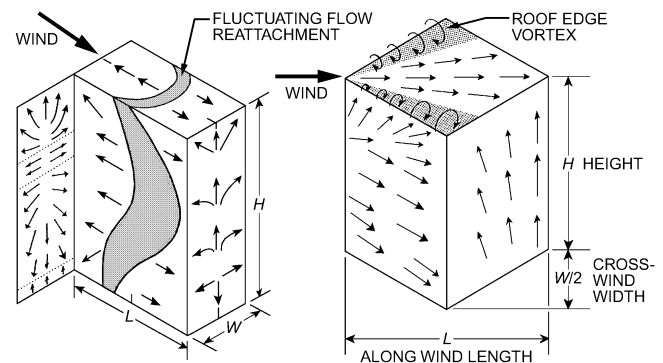**Fig. 4   Flow Patterns Around Rectangular Building**

Fig. 5   Surface Flow Patterns and Building Dimensions

produce odors. Air intakes should also not be placed near traffic or truck waiting areas. General building exhausts should also not be placed near outside contamination sources because flow reversal and ingestion of air through exhaust outlets can occur under some conditions (Seem et al. 1998).

Examining airflow around a building can help determine air intake placement. When wind is perpendicular to the upwind wall, air flows up and down the wall, dividing at about two-thirds up the wall (Figures 4 and 5). The downward flow creates ground-level swirl (shown in Figure 4) that stirs up dust and debris. To take advantage of the natural separation of wind over the upper and lower half of a building, toxic or nuisance exhausts should be located on the roof and intakes located on the lower one-third of the building, but high enough to avoid wind-blown dust, debris, and vehicle exhaust. If ground-level sources (e.g., wind-blown dust and vehicle exhaust) are major sources of contamination, rooftop intake is desirable.

Code Requirements for Air Intakes

Many model building codes exist, and local governments adopt and amend codes as needed. Architects and building systems designers need to be familiar with local and national codes applicable to each project. Mechanical and plumbing codes typically give minimum required separation distances for some situations. However, maintaining these separation distances does not necessarily guarantee that intake contamination will not occur.

One example of a model building code is the *Uniform Mechanical Code* (UMC) [IAPMO 1997a], which has been widely adopted in the United States. The UMC requires that exhausts be at least 0.9 m from property lines and 0.9 m from openings into buildings. Makeup air intakes should be placed to avoid recirculation. Grease and explosives-bearing ducts, combustion vents, and refrigeration equipment have special requirements: intakes should be at least 3 m from combustion vents, plumbing vents, and exhaust air outlets, and be at least 3 m above a road. Cooling towers should be 1.5 m above or 6 m away from intakes.

The *Uniform Plumbing Code* (UPC) [IAPMO 1997b], requires that exhaust vents from domestic water heaters be 0.9 m or more above air inlets. Sanitary vents must be 3 m or more from or 0.9 m above air intakes. When UPC and UMC requirements conflict, the UPC provisions govern. However, local jurisdictions may modify codes, so the adopted versions may have significantly different requirements than the model codes.

Treatment and Control Strategies

When available intake-exhaust separation does not provide the desired dilution factor, or intakes must be placed in undesirable locations, ventilation air requires some degree of treatment, as discussed in Section 6.1.1 of ASHRAE *Standard* 62-2001. Fibrous media, inertial collectors, and electrostatic air cleaners, if properly selected, installed, and maintained, can effectively treat airborne particles. Reducing gaseous pollutants requires scrubbing, absorptive, adsorptive, or incinerating techniques. Biological hazards require special methods such as using high-efficiency particulate air (HEPA) filters and ultraviolet light. Chapters 24 and 25 of the 2000 *ASHRAE Handbook—HVAC Systems and Equipment* describe these treatments in detail. One control approach that should be used with care is selective operation of intakes. If a sensor in the intake air stream detects an unacceptable level of some substance, the outside air dampers are closed until the condition passes. This strategy has been used for helicopter landing pads at hospitals and during emergency generator testing. The drawbacks are that pressurization is lost and ventilation air is not provided unless the recirculated air is heavily treated. In areas of chronically poor outside air quality, such as large urban areas with stagnant air, extensive and typically costly treatment of recirculated air may be the only effective option when outside air dampers are closed for extended periods.

## Intake Locations for Heat-Rejection Devices

Cooling towers and similar heat-rejection devices are very sensitive to airflow around buildings. This equipment is frequently roof-mounted, with equipment intakes close to the roof where air can be considerably hotter and at a higher wet-bulb temperature than air that is not affected by the roof. This can reduce the capacity of cooling towers and air-cooled condensers.

Heat exchangers often take in air on one side and discharge heated, moist air horizontally from the other side. Obstructions immediately adjacent to these horizontal-flow cooling towers can drastically reduce equipment performance by reducing airflow. Exhaust to intake recirculation can be a serious problem for equipment that has an intake and exhaust on the same housing. Recirculation is even more serious than reduction in airflow rate for such devices. Recirculation of warm, moist exhaust raises the inlet wet-bulb temperature, which reduces performance. Recirculation can be caused by adverse wind direction, local disturbance of the airflow by an upwind obstruction, or by a close downwind obstruction. Vertical exhaust ducts may need to be extended to reduce recirculation and improve equipment effectiveness.

Wind Recirculation Zones on Flat-Roofed Buildings

Stack height design must begin by considering the wind recirculation regions (Figure 6). To avoid exhaust reentry, the stack plume must avoid rooftop air intakes and wind recirculation regions on the roof and in the wake downwind of the building. Where capped stacks or exhaust vents discharge within this region, gases rapidly diffuse to the roof and may enter ventilation intakes or other openings. Figures 4 and 6 show that exhaust gas from an improperly designed stack is entrained into the recirculating flow zone behind the downwind face and is brought back into contact with the building.

Wilson (1979) found that, for a flat-roofed building, the upwind roof edge recirculation region height H_c at location X_c and its recir-
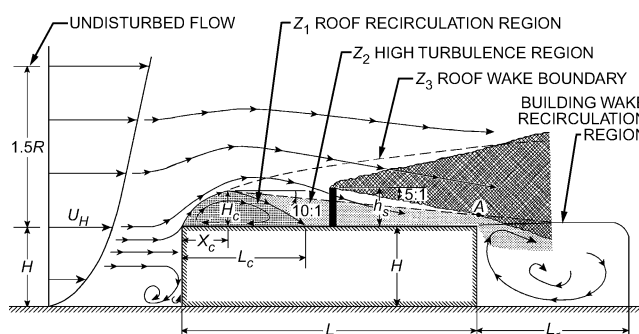
Fig. 6   **Design Procedure for Required Stack Height to Avoid Contamination**
(Wilson 1979)

culation length L_c (shown in Figures 1 and 6) are proportional to the building size scale R:

$$H_c = 0.22R \tag{1}$$

$$X_c = 0.5R \tag{2}$$

$$L_c = 0.9R \tag{3}$$

and the wind recirculation cavity length L_r on the downwind side of the building is approximately

$$L_r = R \tag{4}$$

where R is the building scaling length:

$$R = B_s^{0.67} B_L^{0.33} \tag{5}$$

where B_s is the smaller of the building upwind face dimensions (height or width) and B_L is the larger. These equations are approximate but are recommended for use. The dimensions of flow recirculating zones depend on the amount of turbulence in the approaching wind. High levels of turbulence from upwind obstacles can decrease the coefficients in Equations (1) to (4) by up to a factor of two. Turbulence in the recirculation region and in the approaching wind also causes considerable fluctuation in the position of flow reattachment locations (Figures 5 and 6).

Rooftop obstacles such as penthouses, equipment housings, and architectural screens are accounted for in stack design by calculating the scale length R for each of these rooftop obstacles from Equation (5) using the upwind face dimensions of the obstacle. The recirculation regions for each obstacle are then calculated from Equations (1) to (4). When a rooftop obstacle is close to the upwind edge of a roof or near another obstacle, the flow recirculation zones interact. Wilson (1979) gives methods for dealing with these situations.

Building-generated turbulence is confined to the roof wake region, whose upper boundary Z_3 in Figure 6 is

$$Z_3/R = 0.28(X/R)^{0.33} \tag{6}$$

where x is the distance from the upwind roof edge where the recirculation region forms. Building-generated turbulence decreases with increasing height above roof level. At the edge of the rooftop wake boundary Z_3, the turbulence intensity is close to the background level in the approach wind. The high levels of turbulence in the air below the boundary Z_2 in Figure 6 rapidly diffuse exhaust gases downward to contaminate roof-level intakes. As shown in Figure 6, the boundary Z_2 of this high-turbulence region downwind of a wind recirculation region is approximated by a straight line

sloping at 10:1 downward from the top of the wind recirculation zone to the roof. The stack in Figure 6 may be inadequate because at point A the plume intersects the high turbulence boundary Z_2. The geometric method for stack height is discussed in more detail in the next section.

GEOMETRIC METHOD FOR ESTIMATING STACK HEIGHT

This section presents a method of specifying stack height h_s so that the lower edge of the exhaust plume lies above air intakes and wind recirculation zones on the roof and downwind of the emitting building, based on flow visualization studies (Wilson 1979). This method does not calculate exhaust dilution in the plume; instead, it estimates the size of recirculation and high turbulence zones, and the stack height to avoid contamination is calculated from the shape of the exhaust plume. High vertical exhaust velocity is accounted for with a plume rise calculation that shifts the plume upward. Low vertical exhaust velocity that allows stack wake downwash of the plume (Figure 3) is accounted for by reducing the effective stack height.

This stack height should prevent reentry of exhaust gas into the emitting building most of the time, provided no large buildings, structures, or terrain are nearby to disturb the approaching wind. The geometric method considers only intakes on the emitting building. Additional stack height or an exhaust-to-intake roof-level dilution calculation is often required if the exhaust plume can impinge on a nearby building (Wilson et al. 1998b). Dilution calculations should be used if this method produces an unsatisfactorily high stack, or if exhaust gases are highly toxic releases from fume hood exhaust.

Rooftop obstacles can significantly alter dispersion from exhaust stacks immediately downwind of the obstacles and of similar height to the obstacles (Stathopoulos et al. 2002). The goal of the geometric stack method is to ensure that the exhaust plume is well above the recirculation zones associated with these obstacles.

Step 1. Use Equations (1) to (5) to calculate the height and location of flow recirculation Zones 1 and 2 and the recirculation zone downwind of the building (see Figure 6). All zones associated with rooftop obstacles up- and downwind of the stack location should be included. Note that Zone 3 is not used in the geometric design method.

Step 2. Calculate the height h_{sc} of a stack with a rain cap and, therefore, no plume rise. The h_{sc} required to avoid excessive exhaust gas reentry is estimated by assuming that the plume spreads up and down from h_{sc} with a 1:5 slope (11.3°), as shown in Figure 6. (This slope represents a downward spread of approximately two standard deviations of a bell-curve Gaussian plume concentration distribution in the vertical direction.) Draw the recirculation regions on the top and downwind sides of penthouses, equipment housings, architectural screens, and other rooftop obstacles upwind and downwind of the stack location. If there are intakes on the downwind wall of the building, include the building recirculation region L_r on this wall. Next, draw a line sloping down at 1:5 in the wind direction above the roof, and slide it downward as shown in Figure 1 until it contacts any one of the recirculation zones on any obstacle upwind or downwind of the stack (or until the line contacts any portion of the building if there are no rooftop zones or sidewall intakes). With the line in this position, its height at the stack location is the smallest allowable plume height h_{sc} for that wind direction. Repeat for other wind directions to find the worst-case (highest) required plume height.

Step 3. Reduce the stack height to give credit for plume rise from uncapped stacks. Only jet momentum rise is used; buoyancy rise is considered as a safety factor. For an uncapped stack of diameter d_e, plume rise h_r from the vertical jet momentum of the exhaust is estimated from Briggs (1984) as

$$h_r = 3.0 \beta d_e (V_e / U_H) \tag{7}$$

where

$$d_e = \sqrt{4A_e / \pi} \tag{8}$$

For an uncapped stack, the capping factor is $\beta = 1.0$. For a capped stack, $\beta = 0$, so $h_r = 0$, and no credit is given for plume rise. U_H is the maximum design wind speed at roof height for which air intake contamination must be avoided. This maximum design speed must be at least as large as the hourly wind speed exceeded 1% of the time. This 1% design speed is listed for many cities in Tables 1A, 2A, and 3A of Chapter 27 of the 2001 *ASHRAE Handbook—Fundamentals*. For cities not on this list, set U_H equal to 2.5 times the annual average hourly wind speed as recommended in Table 2 of Chapter 16 of the 2001 *ASHRAE Handbook—Fundamentals*.

Step 4. Increase stack height, if necessary, to account for stack wake downwash caused by low exhaust velocity, as described in the section on Recommended Stack Exhaust Velocity. For a vertically directed jet from an uncapped stack ($\beta = 1.0$), Wilson et al. (1998b) recommend a stack wake downwash adjustment h_d of

$$h_d = d_e(3.0 - \beta V_e / U_H) \tag{9}$$

for $V_e / U_H < 3.0$. For $V_e / U_H > 3.0$, there is no downwash and $h_d = 0$. Rain caps and louvers are frequently used on stacks of gas- and oil-fired furnaces and packaged ventilation units, for which $\beta = 0$ and $h_d = 3.0d_e$.

The final adjusted stack height h_s recommended is

$$h_s = h_{sc} - h_r + h_d \tag{10}$$

The advantage of using an uncapped stack instead of a capped stack is considerable. If the minimum recommended exhaust velocity V_e of $1.5U_H$ is maintained for an uncapped stack ($\beta = 1.0$), plume downwash $h_d = 1.5d_e$ and $h_r = 4.5d_e$. For a capped stack ($\beta = 0$), $h_d = 3.0d_e$ and $h_r = 0$. Using these values in Equation (10), an uncapped stack can be made $6.0d_e$ shorter than a capped stack.

Example 1. The stack height h_s of the uncapped vertical exhaust on the building in Figure 1 must be specified to avoid excessive contamination of intakes A and B by stack gases. The stack has a diameter d_e of 0.5 m and an exhaust velocity V_e of 9.0 m/s. It is located 16 m from the upwind edge of the roof. The penthouse's upwind wall (with intake A) is located 30 m from the upwind edge of the roof, 4 m high, and 7 m long in the wind direction. The top of intake A is 2 m below the penthouse roof. The building has a height H of 15 m and a length of 62 m. The top of intake B is 6 m below roof level. The width (measured into the page) of the building is 50 m, and the penthouse is 9 m wide. The annual average hourly wind speed is 12.8 km/h at a nearby airport with an anemometer height H_{met} of 10 m. The building is in suburban terrain (Category 2 in Table 1 of Chapter 16 of the 2001 *ASHRAE Handbook—Fundamentals*). Calculate the required stack height h_s by the geometrical method using the lowest allowable design wind speed.

Solution: The first step is to set the height h_{sc} of a capped stack by projecting lines with 1:5 slopes so that recirculation zones are covered, as shown in Figure 1. The only influence of intake location is that the downwind recirculation zone must be considered if there is an intake on the downwind wall, which is true for intake B in this example.

First, check the rooftop recirculation zone associated with the penthouse. To find the height of this recirculation zone, use Equation (5):

$$R = (4)^{0.67}(9.0)^{0.33} = 5.23 \text{ m}$$

Then use Equations (1) and (2):

$$H_c = (0.22)(5.23) = 1.15 \text{ m}$$

$$X_c = (0.5)(5.23) = 2.62 \text{ m}$$

With the 1:5 slope of the lower plume boundary shown in Figure 6, the capped stack height in Figure 1 (measured from the main roof) must be

$$h_{sc} = 0.2(30 - 16 + 2.62) + 1.15 + 4.0 = 8.5 \text{ m}$$

to avoid the recirculation zone above the penthouse.

Next, check the building wake recirculation zone downwind of the building. The plume must also avoid this region because intake B is located there. The length of this recirculation region is found using Equation (4):

$$L_r = (15)^{0.67}(50)^{0.33} = 22.3 \text{ m}$$

Projecting the downwind corner of this recirculation region upwind with a 1:5 slope to the stack location gives the required height of a no-downwash capped stack above the main roof level as

$$h_{sc} = 0.2(62 + 22.3 - 16) = 13.7 \text{ m}$$

for the plume to avoid the recirculation zone on the downwind side of the building.

The design stack height is set by the condition of avoiding contamination of the building wake, because avoiding the penthouse roof recirculation requires only a 8.5 m capped stack. Credit for plume rise h_r from the uncapped stack requires calculation of the building wind speed U_H at $H = 15$ m. The minimum allowable design wind speed is the speed that is exceeded 1% of the time at the meteorological station. From Table 2 in Chapter 16 of the 2001 *ASHRAE Handbook—Fundamentals*, this is found by multiplying the hourly average wind speed by a factor of 2.5. In this case, for $H_{met} = 11.6$ m at the airport meteorological station, this 1% wind speed is $U_{met} = 2.5(12.8) = 32$ km/h = 9 m/s. With the airport in open terrain (Category 3 of Table 1 of Chapter 16 of the 2001 *ASHRAE Handbook—Fundamentals*), and the building in urban terrain (Category 2), the wind speed adjustment parameters are $a_{met} = 0.14$ and $\delta_{met} = 274$ m at the airport, and $a = 0.22$ and $\delta = 365$ m at the building. Using Equation (4) in Chapter 16 of the 2001 *ASHRAE Handbook—Fundamentals*, with building height $H = 15$ m,

$$U_H = 9\left(\frac{274}{11.6}\right)^{0.14}\left(\frac{15}{365}\right)^{0.22} = 7.0 \text{ m/s}$$

Because $V_e/U_H = 9.0/7.0 = 1.28$ is less than 3.0, there is some plume downwash as shown in Figure 3. From Equation (9),

$$h_d = 0.5[3 - 10(1.28)] = 0.86 \text{ m}$$

Then, using Equation (7), the plume rise at design wind speed is

$$h_r = 3.0(0.5)(1.28) = 1.92 \text{ m}$$

Using these values in Equation (10), the uncapped height h_{sc} is, with the height reduction credit for the 1.92 m rise and the height addition to account for the 0.86 m downwash,

$$h_s = 13.7 - 1.92 + 0.86 = 12.64 \text{ m}$$

As shown in Figure 1, this stack height is measured above the main roof. If the stack height is higher than desirable, an alternative is to use dilution calculations. The geometric method does not directly account for dilution within the plume.

EXHAUST-TO-INTAKE DILUTION CALCULATIONS

Worst-Case Critical Dilution

This section describes a method for computing outside dilution of exhausts emitted from a rooftop stack. The resulting dilution can be converted to contaminant concentration for comparison to odor thresholds or health limits. The results and equations given were obtained from wind tunnel studies of simple building shapes.

Dispersion of pollutants from building exhaust depends on the combined effect of atmospheric turbulence in the wind approaching the building and turbulence generated by the building itself. This building-generated turbulence is most intense in and near the flow recirculation zones that occur on the upwind edges of the building (Figures 1 and 5). Dilution of exhaust gas is estimated using design procedures developed for tall isolated stacks (EPA 1995), with modifications to include the high turbulence levels experienced by a plume diffusing over a building roof in an urban area. Halitsky (1982), Hosker (1984), Meroney (1982), and Wilson and Britter (1982), review gas diffusion near buildings.

The geometric stack design procedure does not give a quantitative estimate of the worst-case critical dilution factor D_{crit} at an air intake. If a required dilution can be specified with known stack emissions and required health limits, odor thresholds, or air quality regulations, computing critical dilutions can be an alternative for specifying stack heights. Petersen and Ratcliff (1991), and Smeaton et al. (1991) discuss the use of emission information and the formulation of dilution requirements in more detail. Exhaust from a single-source dedicated stack may require more atmospheric dilution than a single stack with the same exhausts combined because emissions are diluted in the exhaust manifold.

Dilution and Concentration Definitions

A building exhaust system releases a mixture of building air and pollutant gas at concentration C_e (mass of pollutant per volume of air) into the atmosphere through a stack or vent on the building. The exhaust mixes with atmospheric air to produce a pollutant concentration C, which may contaminate an air intake or receptor if the concentration is larger than some specified allowable value C_{allow} (Figure 4). The dilution factor D between source and receptor mass concentrations is defined as

$$D = C_e/C \tag{11}$$

where

C_e = contaminant mass concentration in exhaust, kg/m³
C = contaminant mass concentration at receptor, kg/m³

The dilution increases with distance from the source, starting from its initial value of unity. If C is replaced by C_{allow} in Equation (11), the atmospheric dilution D_{req} required to meet the allowable concentration at the intake (receptor) is

$$D_{req} = C_e/C_{allow} \tag{12}$$

The exhaust (source) concentration is given by

$$C_e = \dot{m}/Q_e = \dot{m}/(A_e V_e) \tag{13}$$

where

$\dot{m}$ = contaminant mass release rate, kg/s
$Q_e = A_e V_e$ = total exhaust volumetric flow rate, m³/s
A_e = exhaust face area, m²
V_e = exhaust face velocity, m/s

The concentration units of mass per mixture volume are appropriate for gaseous pollutants, aerosols, dusts, and vapors. The concentration of gaseous pollutants is usually stated as a volume fraction f (contaminant volume/mixture volume), or as ppm (parts per million) if the volume fraction is multiplied by 10^6. The pollutant volume fraction f_e in the exhaust is

$$f_e = Q/Q_e \tag{14}$$

where Q is the volumetric release rate of the contaminant gas. Both Q and Q_e are calculated at exhaust temperature T_e.

The volume concentration dilution factor D_v is

$$D_v = f_e/f \tag{15}$$

where f is the contaminant volume fraction at the receptor. If the exhaust gas mixture has a relative molecular mass close to that of air, D_v may be calculated from the mass concentration dilution D by

$$D_v = (T_e/T_a)D \tag{16}$$

where

    T_e = exhaust air absolute temperature, K
    T_a = outside ambient air absolute temperature, K

Many building exhausts are close enough to ambient temperature that volume fraction and mass concentration dilutions D_v and D are equal.

Gaussian Plume Equations for Roof-Level Dilution

This section presents equations for predicting worst-case roof-level dilution of exhaust from a vertical stack on a roof. The equations assume a bell-shaped Gaussian concentration profile in both the vertical and cross-wind horizontal directions. Gaussian profiles have been used in many atmospheric dispersion models, such as those used by the U.S. Environmental Protection Agency. Considering their simplicity, bell-shaped Gaussian concentration profiles in the cross-wind y and vertical z directions at a given horizontal distance x represent atmospheric dispersion remarkably well (see Brown et al. 1993).

The dilution equations predict the roof-level dilution D_r, which is the ratio of contaminant concentration C_e at the exit point of the exhaust to the maximum concentration C_r on the plume centerline at roof level, giving $D_r = C_e/C_r$. The centerline of the plume is defined in the x direction, with y the lateral (cross-wind) distance off the plume centerline (axis), and z the vertical. Dilution is affected by three processes:

- Wind carries the plume downwind. The higher the wind speed, the greater the dilution on the plume axis. The wind speed carrying the plume U_H is the wind speed in the undisturbed flow approaching the top of the building assumed to be constant with height for the Gaussian model.
- Wind turbulence spreads the plume vertically and laterally (cross-wind). Plume spreads in the cross-wind y direction and the vertical z direction are σ_y and σ_z. These plume spreads increase with downwind distance.
- The plume is carried vertically by the initial buoyancy and vertical momentum of the exhaust at the stack exit. The higher the plume, the greater the dilution at the roof surface. The stronger the wind, the less the plume rises, which may produce less dilution.

Thus, wind speed has two influences: (1) at very low wind speed, the exhaust jet from an uncapped stack rises high above roof level, producing a large exhaust dilution D_r at a given intake location; and (2) at high wind speed, the dilution is also large because of longitudinal stretching of the plume by the wind. Between these extremes is the critical wind speed $U_{H,crit}$, at which the smallest amount of dilution occurs for a given exhaust and intake location.

Contaminant dilution measured at an intake depends on the height h of the exhaust plume above the roof. Dilution at roof level D_r is inversely proportional to the volume flow rate of effluent from the stack, $Q_e = \pi V_e d_e^2/4$, and directly proportional to the wind speed U_H that stretches the plume longitudinally in the x direction. Dilution at roof level in a Gaussian plume emitted at the final rise plume height of h is

$$D_r = 4 \frac{U_H}{V_e} \frac{\sigma_y}{d_e} \frac{\sigma_z}{d_e} \exp\left[\frac{h^2}{2\sigma_z^2}\right] \tag{17}$$

where

$$h = h_s + h_r - h_d \tag{18}$$

where the plume rise h_r and stack wake downwash h_d are calculated from Equations (7) and (9). The stack height h_s in Equation (18) is

the height of the stack tip above the roof, minus the height at the intake location of the rooftop obstacles and recirculation zones. If exhaust gases are hot, buoyancy increases the rise of the exhaust gas mixture and produces lower concentrations (higher dilutions) at roof level. For all exhausts except very hot flue gases from combustion appliances, it is recommended that plume rise from buoyancy be neglected in dilution calculations and stack design on buildings. By neglecting buoyant plume rise, Equation (17) for roof-level dilution D_r has an inherent safety factor, particularly at low wind speed, where buoyancy rise is significant.

Limiting Contribution of Plume Rise to D_r Near Stacks

Close to the stack, the ratio $h^2/2\sigma_z^2$ in Equation (17) becomes very large, causing the exponential term in Equation (17) to over-predict the roof-level dilution factor D_r. Preventing this requires that the value of $h^2/2\sigma_z^2$ must not be allowed to exceed 5.0. This upper limit was suggested by Wilson et al. (1998a) based on their water channel scale model experiments. Maintaining $h^2/2\sigma_z^2 < 5.0$ limits the amount of dilution allowed due to plume rise to $\exp(5.0) = 148$ near the stack. Limiting $h^2/2\sigma_z^2$ to 5.0 means h is limited to $h = 3.16\sigma_z$. In effect, this limits Equation (17) to an effective plume height no more than three vertical plume standard deviations σ_z above the $h_s = 0$ plane.

Smallest Plume Height h_{small} for Dilution Calculations

Equations (17) and (18) apply only if the exhaust plume avoids all obstacles and flow recirculation zones between the stack and air intake. The procedure for calculating the smallest plume height h_{small} for which the dilution and plume rise equations are valid is similar to the geometric method for stack design. Accurate dilution calculations from Equation (17) can only be made for plumes with combined stack height h_s, plume rise h_r, and downwash h_d in Equation (18) above this smallest height h_{small}. First, determine the critical wind direction on a plan view of the roof by drawing a line through the stack location and the intake at which dilution has been calculated. All obstacles upwind of the air intake location and within one obstacle width laterally of this critical wind direction line are *active* obstacles. To find h_{small}, use the geometric-method plume height including only these active obstacles. Obstacles downwind of the air intake in question and the wake region downwind of the building need not be considered. After design calculations for dilution, and stack height h_s is chosen, the plume height h_{crit} at the critical design wind speed U_H must be compared to h_{small} to determine whether $h_{crit} > h_{small}$. If the proposed stack produces a plume height larger than h_{small}, the dilution calculation is valid.

If the plume height is less than h_{small} but higher than any rooftop obstacle or rooftop recirculation zone (h_{top} in Figure 1), then only the physical stack height above h_{top} should be used to compute plume height rather than the full physical stack height. If the plume height does not reach h_{top}, use Equation (22) for a flush vent with no plume rise to approximate the exhaust to intake dilution.

Cross-Wind and Vertical Plume Spreads for Dilution Calculations

Equations for vertical and cross-wind spread were developed for nonbuoyant exhaust jets from rooftop stacks on flat-roofed buildings (Wilson et al. 1998a). In the first 300 m downwind from the stack, both cross-wind plume spread σ_y and vertical plume spread σ_z increase almost linearly with distance x. The recommended equations for plume spreads are based on full-scale atmospheric measurements by McElroy and Pooler (1968) in an urban area, as used in the EPA (1995) model ISCST. The urban ISCST equations are adjusted here from the 60 min measured averaging time to 2 min averages with the 0.2 power law applied to both vertical and cross-wind spreads. Then, the vertical spread over a building roof is

assumed to remain constant at the 2 min averaging time value for longer averaging times. The plume equations are as follows:

$$\frac{\sigma_y}{d_e} = 0.071\left(\frac{t_{avg}}{2.0}\right)^{0.2}\frac{X}{d_e} + \frac{\sigma_o}{d_e} \qquad (19)$$

$$\frac{\sigma_z}{d_e} = 0.071\frac{X}{d_e} + \frac{\sigma_o}{d_e} \qquad (20)$$

where t_{avg} is the concentration averaging time in minutes, X is the distance downwind from the stack, and σ_o is the initial source size that accounts for stack diameter and for dilution jet entrainment during plume rise.

The dependence of initial spread σ_o on exit velocity to wind speed ratio V_e/U_H is

$$\frac{\sigma_o}{d_e} = \left[0.125\beta\frac{V_e}{U_H} + 0.911\beta\left(\frac{V_e}{U_H}\right)^2 + 0.250\right]^{0.5} \qquad (21)$$

where β is the rain cap factor: $\beta = 1$ for no rain cap, and $\beta = 0$ if there is a rain cap. For $\beta = 0$, there is still an effective source size σ_o equal to half the diameter d_e of the stack.

The averaging time over which exhaust gas concentration exposures are measured is important in determining roof-level dilution. As averaging time increases, the exhaust gas plume meanders more from side to side, reducing the time-averaged concentration (and increasing the dilution) observed at an air intake location. The effect of changing the averaging time over a range of about 2 to 180 min can be estimated by adjusting the 2 min value of the cross-wind spread σ_y by the 0.2 power of the averaging time t_{avg} (Wollenweber and Panofsky 1989). This averaging time adjustment appears directly in Equation (19). If the exhaust and intake are both located in the same flow recirculation region, dilution is less sensitive to averaging time than predicted by the 0.2 power law. For the case of both stack tip and air intake in the same wind recirculation zone, assume the D_r values for 2 min averages also apply for all averaging times from 2 to 60 min.

Equations (17), (18), and (19) imply that dilution does not depend on the location of either the exhaust or intake, only on the horizontal distance X between them and the stack height h_s. This is reasonable when both exhaust and intake locations are on the same building wall or on the roof. Dilution can increase if the intake is on the wall and the exhaust stack is located on the roof, but at present there are no reliable estimates for this effect on stack exhaust.

Stack Design Using Dilution Calculations and Charts for Critical Wind Speed

Starting with the volume flow rate Q_e and exit diameter d_e of an exhaust stack, dilution calculations can be used to select the design stack height h_s required to produce a specified minimum exhaust-to-intake dilution D at horizontal distance X from the stack. First, the exhaust velocity at the stack tip is calculated from $Q_e = \pi V_e d_e^2/4$. Then, the geometric design method is used to determine the smallest plume height h_{small} for which the dilution equations are valid. Determining the stack height is a trial-and-error procedure in which a first guess is made for the stack height and dilution is calculated for several wind speeds to determine the worst-case critical wind speed $U_{H,crit}$ at which the minimum dilution D_{crit} occurs. Starting with a high U_H (e.g., the speed exceeded less than 1% of the time) a spreadsheet is used to calculate the plume rise h_r from Equation (8), downwash h_d from Equation (9), and plume spreads σ_o, σ_y, and σ_z. Using the first guess for stack height h_s, Equation (18) is used to calculate plume height h. If this height $h > h_{small}$, Equation (17) is used to calculate the roof-level dilution at the air intake. Note that when $h^2/2\sigma_z^2$ is calculated, it must be limited to a maximum of 5.0 in

Equation (17). D_r is then recalculated for a range of U_H to determine the critical wind speed at which minimum dilution D_{crit} occurs. If D_{crit} is too high or too low, h_s is adjusted and the dilution calculations repeated to find a new critical wind speed and dilution.

The charts for four different heights of uncapped stacks (Figure 7) can be used to speed up calculation of h_s. This procedure begins with a first guess for stack height h_s and calculating the ratio of stack height to inside diameter h_s/d_e and of the exhaust to intake distance X/h_s. The two charts with h_s/d_e ratios higher and lower than this first guess are used to read up to the lowest V_e/U_H curve at that X/h_s to find the minimum dilution D_{crit} and critical exhaust velocity ratio $V_e/U_{H,crit}$. Linear interpolation using h_s/d_e between values from the two charts is used to find the D_{crit} and $V_e/U_{H,crit}$ for the first-guess stack height. If this critical dilution is too low or too high, the stack height is adjusted for the second guess and the procedure is repeated until the desired stack height is found.

Figure 8 is a design chart for dilution from capped stacks ($\beta = 0$) with no plume rise. For capped stacks, the critical wind speed for minimum dilution at an intake is related to increased plume spread observed at low wind speeds rather than the competing effects of plume rise versus wind dilution. After making a first guess for stack height, the minimum critical dilution for capped stacks can be calculated directly using the a value $U_{H,crit} = 2$ m/s. This is based on the observation that, for wind speeds less than 2 m/s at roof height, the atmosphere tends to develop high levels of turbulence that cause plume meandering and increase exhaust-to-intake dilution.

Example 2. Using the same building geometry as in Example 1, calculate the dilution for a shorter stack with $h_s = 8.5$ m above the main roof. The stack has a diameter d_e of 0.5 m and an exhaust velocity V_e of 9 m/s. The stack gas concentration must be diluted by 1800:1 to be considered safe for 2 min exposures at intakes A and B. (This required dilution is determined from occupational health standards and estimated emission rates.) Using the dilution charts, calculate the critical roof-level dilution factor D_{crit} and critical wind speed $U_{H,crit}$ for contamination for intakes A and B. Is the stack height of 8.5 m sufficient to handle this toxic substance?

Solution:

Intake A: Equation (17) applies to intakes on the roof surface. In this example, intake A is some height above the main rooftop on the side of the penthouse. For intake A with this configuration, it is recommended to use a fictitious "rooftop" height equal to the top of the penthouse. The physical stack height used in the dilution equations is then measured from the penthouse roof: $8.5 - 4 = 4.5$ m. For intake A there are no recirculation zones or obstructions between the stack and the intake. The penthouse obstruction is downwind of the intake, and the leading edge recirculation zone has reattached before reaching the stack. Thus $h_{small} = 0$ and Equation (17) applies. The horizontal distance from the stack to the intake is $X = 14$ m. The stack height ratio is $h_s/d_e = 4.5/0.5 = 9$, and the exhaust-to-intake distance ratio $X/h_s = 14/4.5 = 3.1$. Then, using Figure 7C for $h_s/d_e = 10$, the critical minimum dilution is 5000, at a critical exhaust velocity to wind speed ratio of about 2.0. Repeating this using Figure 7B for $h_s/d_e = 5$ yields a critical dilution of 280 and a critical exhaust velocity to wind speed ratio of 0.5. Then, interpolating linearly on the height ratio h_s/d_e,

$$D_{A,crit} = 5000 - \frac{(10 - 9.02)}{(10 - 5)}(5000 - 280) = 4075$$

$$\frac{V_e}{U_{H,crit,A}} = 0.5 + \frac{(10 - 9.02)}{(10 - 5)}(2 - 0.79) = 0.6$$

From this velocity ratio the critical wind speed at roof height is $U_{H,crit} = 9/0.79 = 11.4$ m/s for intake A. This high wind speed is likely to occur very rarely. (In Example 1, the hourly average wind speed $U_H = 7.0$ m/s is exceeded only 1% of the time.) With a predicted dilution of 4075:1, the dilution target of 1800:1 is met at intake A.

Intake B: The stack height can be measured above the roof of the building if plume height h_{crit} at the critical wind speed is greater than h_{small} above which the dilution equations and charts are valid; this plume
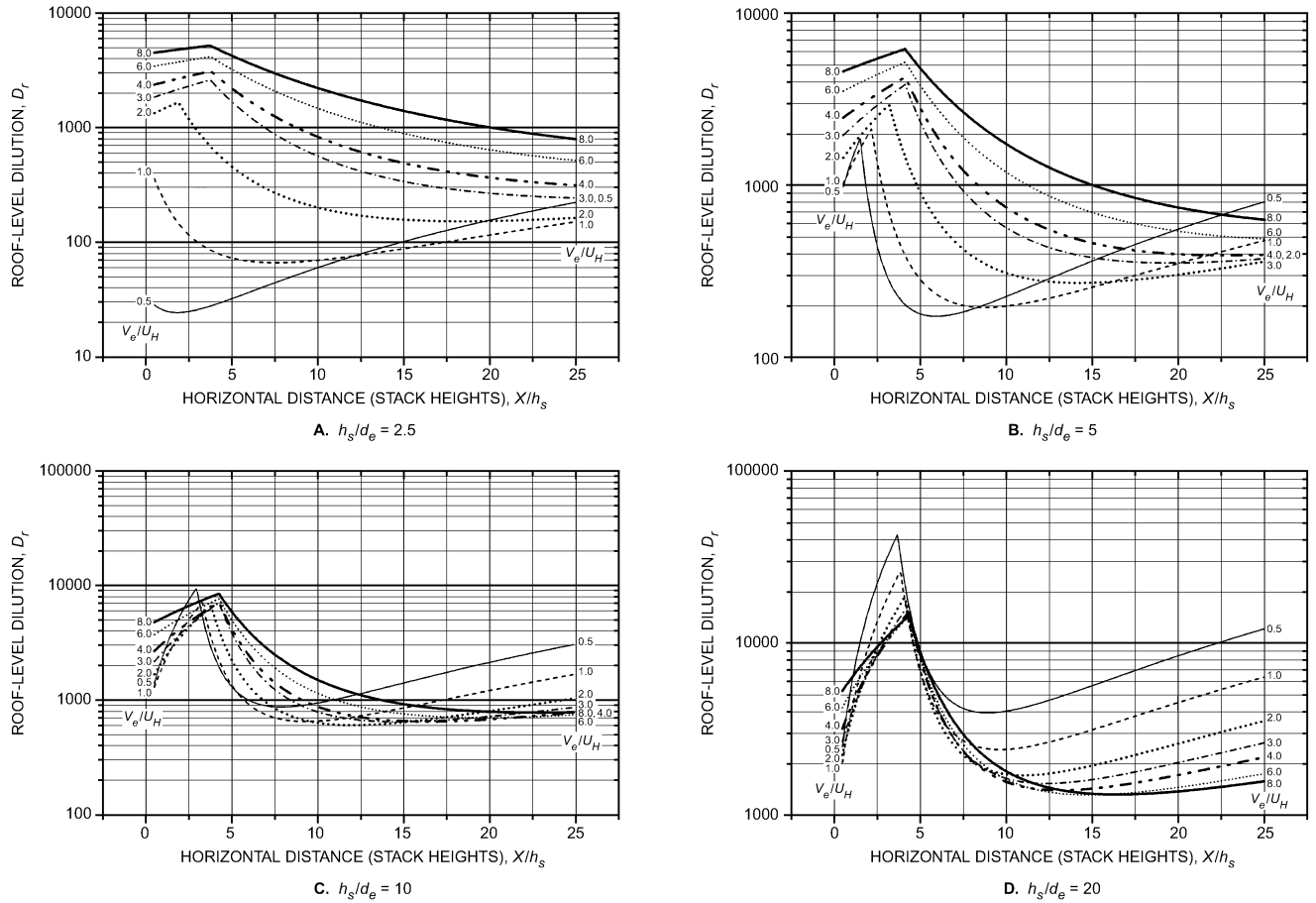
A. $h_s/d_e = 2.5$

B. $h_s/d_e = 5$

C. $h_s/d_e = 10$

D. $h_s/d_e = 20$

Fig. 7   Dilution Versus Distance

height condition will be checked later. Using the stack height above roof level as the effective height for Intake B, $h_s = 8.4$ m, and the horizontal distance from stack to intake is $X = 45.8$ m. The stack height ratio is $h_s/d_e = 8.5/0.5 = 17.0$, and the exhaust-to-intake distance ratio $X/h_s = 45.8/8.5 = 5.39$. Then, using Figure 7D for $h_s/d_e = 20$ the critical minimum dilution is 5000, at a critical exhaust velocity to wind speed ratio of about 2.0. Repeating this using Figure 7C for $h_s/d_e = 10$ yields a critical dilution of 1100 and a critical exhaust velocity to wind speed ratio of 0.5. Then, interpolating linearly on the height ratio h_s/d_e,

$$D_{B,crit} = \left(5000 - \frac{20 - 17}{20 - 10}\right)(5000 - 1100) = 3830$$

$$\frac{V_e}{U_{H,crit,B}} = \left(2 - \frac{20 - 17}{20 - 10}\right)(2 - 0.5) = 1.55$$

From this velocity ratio the critical wind speed at roof height is $U_{H,crit} = 9/1.55 = 5.8$ m/s for intake B. This is moderately high but will occur more than 1% of the time.

The final step for intake B is to use a modified geometric stack design method to check that the plume height under critical wind speed conditions is above the smallest height h_{small} for which the dilution equations are valid. The height h_{small} is determined by projecting a 1:5 slope upwind from the roof level above the wall on which intake B is located, For 45.8 m from the stack to intake B, this produces a height $h_{small} = (0.2)(45.8) = 9.2$ m above the roof at the stack location. The plume height h_{crit} at the critical wind speed for intake B is determined by calculating the plume rise and downwash at the critical exhaust velocity to wind speed ratio of $V_e/U_{H,crit,B} = 1.55$. From Equation (7) for an uncapped stack with $\beta = 1.0$, the rise is $h_r = 3.0(1.0)(0.5)(1.55) = 2.33$ m. The plume downwash at this critical velocity ratio is $h_d = (0.5)[(3 - 1.0(1.55)] = 0.7$ m. From Equation (18), the plume height at
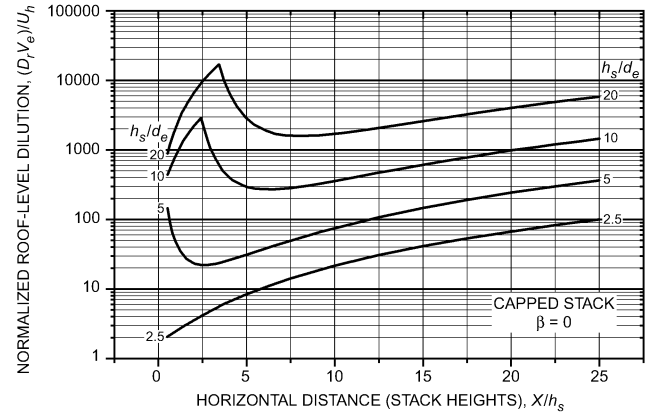

Fig. 8   Dilution Versus Distance for Capped Stack

the critical wind speed for intake B is $h_{crit} = 8.5 + 2.3 - 0.7 = 10.1$ m, which is higher than $h_{small} = 9.2$ m, so the calculations are valid.

In summary, both intake A with a critical dilution of 4075, and intake B with a critical dilution of 3800, meet the health and safety requirement of providing a minimum exhaust-to-intake dilution of at least 1800.

Dilution from Flush Exhaust Vents with No Stack

For exhaust grills and louvers on the roof or walls of a building or penthouse, exhaust height $h = 0$ in Equation (17). Combining Equations (17), (19), and (20) gives

$$D_s = 4 \frac{U_H}{V_e}\left(0.071\left(\frac{t_{avg}}{2.0}\right)^{0.2}\frac{S}{d_e} + \frac{\sigma_o}{d_e}\right)\left(0.071\frac{S}{d_e} + \frac{\sigma_o}{d_e}\right) \quad (22)$$

where the stretched-string distance S between the nearest edge of the exhaust to the nearest edge of the intake replaces the horizontal distance X in the cross-wind and vertical plume spreads σ_y and σ_z in Equations (19) and (20). The concentration averaging time t_{avg} at the intake is in minutes, for the reference averaging time of 2.0 min. The subscript s in the dilution D_s from a surface exhaust distinguishes it from the roof-level dilution D_r from a stack (Equation 17). The initial dilution in the flush-vent exhaust plume can be approximated by an uncapped jet with $\beta = 1.0$ in Equation (21) to calculate the effective source spread σ_o that generates the self-dilution by jet entrainment.

    Minimum critical dilutions for flush exhausts can be calculated using the approximate value $U_{H,crit} = 2$ m/s based on the observation that, for wind speeds less than 2 m/s at roof height, the atmosphere tends to develop high levels of turbulence that increase exhaust-to-intake dilution. For flush roof exhausts with no stack, and for wall intakes, the experiments of Li and Meroney (1983) suggest that D_s at the intake is about a factor of 4 larger than the dilution at a roof-level intake the same stretched-string distance S from the stack.

Example 3. The exhaust flow of $Q_e = 1.76$ m³/s in Example 1 comes from a louvered grill at location A. The exhaust grill is 0.7 m high and 0.7 m wide. What is the critical exhaust-to-intake dilution factor at intake B on the downwind wall of the building for averaging times of 2 min and 60 min?

Solution: Exhaust grill A has a face area of $A_e = 0.49$ m² and an exhaust velocity V_e of 3.59 m/s. From Equation (8), the effective exhaust diameter is $d_e = [(4)(0.49)/\pi]^{0.5} = 0.79$ m. The stretched-string distance S from exhaust A to intake B is the sum of the 2 m from the top of A to the top of the penthouse, plus the 7 m length of the penthouse, plus the sloped line of horizontal length 24.9 m from the downwind edge of the penthouse roof, and a vertical drop of 4 m to the roof, plus the 6 m to intake B:

$$S = 2 + 7 + \sqrt{24.9^2 + (4+6)^2} = 35.8 \text{ m}$$

so that $S/d_e = 35.8/0.79 = 45.3$ m. The critical wind speed is approximately $U_{H,crit} = 2$ m/s for capped stacks and flush vents. The initial plume spread σ_o is calculated from Equation (21) with $V_e/U_H = 3.59/2 = 1.8$ m, and an uncapped exhaust, $\beta = 1.0$,

$$\frac{\sigma_o}{d_e} = \sqrt{0.125(1.0)(1.77) + 0.911(1.0)(1.8)^2 + 0.250} = 1.85$$

The critical dilution of exhaust from A at intake B is calculated from Equation (22):

$$D_{s,crit} = 4\left(\frac{400}{707}\right)\left[0.071\left(\frac{t_{avg}}{2.0}\right)^{0.2}(45.2) + 1.85\right][0.071(45.2) + (1.85)]$$

For an averaging time $t_{avg} = 2$ min, the critical dilution is 57, and 93 for a 60 min averaging time. Because the plume from A passes around the edge of the roof to reach intake B, dilution can be increased by a factor of 4 (Li and Meroney 1983) to obtain $D_{s,crit} = 57(4) = 228$ for 2 min and $D_{s,crit} = 93(4) = 372$ for 60 min. These are conservative estimates because they represent the dilution at a low critical wind speed of 2 m/s. Using the method in Example 1, the annual average hourly wind speed at roof height is 2.8 m/s.

Annual Hours of Occurrence of Highest Intake Contamination

    To assess the severity of the hazard caused by intake contamination, it is useful to know the number of hours per year that exhaust-to-intake dilution is likely to be no more than a factor of two higher than the worst-case minimum dilution D_{crit} calculated at $U_{H,crit}$.

The first step in making a frequency-of-occurrence estimate for the number of low-dilution hours is to use the dilution charts in <u>Figures 7</u> and <u>8</u> to find the range of wind speeds U_H over which the dilution D_r is within a factor of two of D_{crit}. The upper and lower limits of this range are then converted to the upper and lower limits of the meteorological station wind speed U_{met}. Weather data are then used to calculate the number of hours per year that wind speeds fall in this range. This number of hours is multiplied by the fraction of time the local wind direction lies in a sector 22.5° on each side of the line joining the exhaust and intake location.

Combined Exhausts and Ganged Stacks

    When exhaust from several collecting stations is combined in a single vent or in a tight cluster of stacks (as recommended in the section on Exhaust Stack and Air Intake Design Strategies), the exhaust concentration C_e of each contaminant stream decreases by mixing with other exhaust streams, and the plume rise increases due to the higher mass flow in the combined jet. Combined exhaust streams significantly lower roof-level intake concentration C_r compared to that from separate exhausts. Where possible, exhausts should be combined before release to take advantage of this increase in overall dilution.

Influence of Architectural Screens on Exhaust Dilution

    Architectural screens are often placed around rooftop equipment to reduce noise or hide equipment. Unfortunately, these screens interact with windflow patterns on the roof and can adversely affect exhaust dilution and thermal efficiency of equipment inside the screen. This section describes a method to account for these screens by modifying the physical stack height h. Architectural screens generate flow recirculation regions similar to those shown downwind of the building and penthouse in <u>Figure 1</u>. These screens are often made of porous materials with mesh or louvers, which influence the height of the recirculation cavity above the screens.

    To incorporate the effect of architectural screens into existing dilution prediction equations, a stack height reduction factor F_h is introduced. Using the equation developed by Petersen et al. (1998), stack height h_s above the roof must be multiplied by F_h when the stack is enclosed within a screen. The effective stack height $h_{s,eff}$ measured above roof level is

$$h_{s,eff} = F_s h_s \quad (23)$$

    The stack height reduction factor F_h is directly related to the screen porosity P_s. For stack heights above the top of the screen that are less than 2.5 times the height of the screen,

$$F_h = 0.81 P_s + 0.20 \quad (24)$$

where porosity is defined as the fraction of open area to total area:

$$P_s = \frac{\text{Open area}}{\text{Total area}} \quad (25)$$

F_h is applied directly to h_s after the required stack height has been calculated, and should be included where the physical stack height is less than 2.5 times the height of the architectural screen.

Example 4. Calculate the required stack height for an uncapped stack with a height of 4.7 m above roof level, surrounded by a 3 m high, 50% porous architectural screen.

Solution: To determine the effect of the 50% porous screen, use Equation (24) with $P_s = 0.5$

$$F_h = 0.81(0.5) + 0.2 = 0.605$$

The screen has reduced the effective stack height from its actual height of 4.7 m to

$$h_{s,eff} = 0.605(4.7) = 2.84 \text{ m}$$

When the effect of the 50% porous screen is added, the 4.7 m stack height is found to behave like a 2.86 m stack. The actual stack height h_s must be increased to account for the screen's effect. This is most easily done by dividing h_s by the stack height reduction factor:

$$h_{s,corrected} = \frac{h_s}{F_h} = \frac{4.7}{0.605} = 7.8 \text{ m}$$

The corrected 7.8 m high stack effectively behaves like a 4.7 m tall stack, and should produce the same dilution at downwind air intakes

Scale Model Simulation and Testing

For many routine design applications, exhaust dilution can be estimated using the data and equations presented in this chapter, which are based on scale modeling of simple building shapes. However, in critical applications, such as where health and safety or energy costs are of concern, or for complicated building configurations, physical modeling or full-scale field evaluations may be required to obtain more accurate estimates. Measurements on small-scale models in wind tunnels or water channels can provide the required design information. Scale modeling is discussed in Chapter 16 of the 2001 *ASHRAE Handbook—Fundamentals*.

SYMBOLS

A_e = stack or exhaust exit face area, m^2
B_L = larger of two upwind building face dimensions H and W, m
B_s = smaller of two upwind building face dimensions H and W, m
C = contaminant mass concentration at receptor at ambient air temperature T_e, Equation (11), kg/m^3
C_{allow} = allowable concentration of contaminant at receptor, Equation (12)
C_e = contaminant mass concentration in exhaust at exhaust temperature T_e, Equation (11), kg/m^3
d_e = effective exhaust stack diameter, Equation (8), m
D = dilution factor between source and receptor mass concentrations, Equation (11)
D_{crit} = critical dilution factor at roof level for uncapped vertical exhaust at critical wind speed $U_{H,crit}$ that produces smallest value of D_r for given exhaust-to-intake distance S and stack height h_s
D_r = roof-level dilution factor D at given wind speed for all exhaust locations at same fixed distance S from intake, Equation (17)
D_{req} = atmospheric dilution required to meet allowable concentration of contaminant C_{allow}, Equation (12)
D_S = dilution at a wall or roof intake from a flush exhaust grill or louvered exhaust, Equation (22)
D_v = dilution factor between source and receptor using volume fraction concentrations, Equation (15)
f = contaminant volume concentration fraction at receptor; ratio of contaminant gas volume to total mixture volume, Equation (15), ppm $\times 10^{-6}$
f_e = contaminant volume concentration fraction in exhaust gas; ratio of contaminant gas volume to total mixture volume, Equation (14), ppm $\times 10^{-6}$
F_h = stack height adjustment factor to adjust existing stack height above screen for influence of screen of exhaust gas dilution, Equation (24)
h_{crit} = height of plume above roof level with plume rise and downwash calculated at the critical wind speed U_{crit}, m
h_d = downwash correction to be subtracted from stack height, Equation (9), m
h_r = plume rise of uncapped vertical exhaust jet, Equation (7), m
h_s = exhaust stack height (typically above roof unless otherwise specified), m
h_{sc} = required height of capped exhaust stack to avoid excessive intake contamination, Equation (10), m
$h_{s,eff}$ = effective exhaust stack height above roof on which it is located, corrected for an architectural screen surrounding the stack, Equation (23) m
h_{small} = minimum plume height above roof level above which dilution Equation (17) is valid, m
H_c = maximum height above roof level of upwind roof edge flow recirculation zone, Equation (1), m

L = length of building in wind direction, Figure 5, m
L_c = length of upwind roof edge recirculation zone, Equation (3), m
L_r = length of flow recirculation zone behind rooftop obstacle or building, Equation (4), m
$\dot{m}$ = contaminant mass release rate, Equation (13), kg/s
P_s = porosity of an architectural screen near a stack, Equation (25)
Q = contaminant volumetric release rate, Equation (14), m^3/s
Q_e = total exhaust volumetric flow rate, Equation (13), m^3/s
R = scaling length for roof flow patterns, Equation (5), m
S = stretched-string distance; shortest distance from exhaust to intake over obstacles and along building surface, Equation (22), m
t_{avg} = time interval over which receptor (intake) concentrations are averaged in computing dilution, Equation (19), min
T_a = outdoor ambient air absolute temperature, Equation (16), K
T_e = exhaust air mixture absolute temperature, Equation (16), K
U_H = mean wind speed at height H of upwind wall in undisturbed flow approaching building, Equation (7), m/s
$U_{H,crit}$ = critical wind speed that produces smallest roof-level dilution factor D_{crit} for uncapped vertical exhaust at given X and h_s, m/s
V_e = exhaust gas velocity, Equation (13), m/s
W = width of upwind building face, m
x = horizontal distance in the direction of the wind, m
X = downwind horizontal distance from center of stack, Equations (19) and (20), m
X_c = distance from upwind roof edge to H_c, Equation (2), m
y = cross-wind distance off the plume centerline, m
z = vertical distance, m
Z_1 = height of flow recirculation zone boundary above roof, Figure 4, m
Z_2 = height of high turbulence zone boundary above roof, Figure 6, m
Z_3 = height of roof edge wake boundary above the roof, Equation (6) and Figure 6, m
β = capping factor; 1.0 for vertical uncapped roof exhaust; 0 for capped, louvered, or downward-facing exhaust
σ_o = standard deviation of initial plume spread at the exhaust used to account for initial dilution, Equation (19), m
σ_y = standard deviation of cross-wind plume spread, Equation (19), m
σ_z = standard deviation of vertical plume spread, Equation (20), m

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